AustinPower Engineering	PEM Fuel Ce Analysis	Il System Manufacturing Cost s for Automotive Applications
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Have been working on fuel cell manufacturing cost modeling for US DOE, UK Carbon Trust, and commercial clients since 2002.





### Approach Manufacturing Cost Modeling Methodology

This approach has been used successfully for estimating the cost of various technologies for commercial clients and the DOE.



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Engineering

Combining performance and cost model will easily generate cost results, even when varying the design inputs.



### The bottom-up cost approach will be used to capture accurately the manufacturing costs for each fabrication step.



# True-value-mapping analysis virtualizes costs in each fabrication step, which breaks down costs into materials, labor, capex, utility, maintenance, etc.



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### Austin Power Engineering's manufacturing cost models can be used to determine a fully loaded selling price to consumers at high or low volumes.



We assume 100% financing with an annual discount rate of 10%, a 10-year equipment life, a 25-year building life, and three months working capital.



### Approach Scope

Our cost assessment includes a fuel cell system, an on-board H2 storage, and a hybrid battery pack which is for a middle size passenger vehicle.

PEMFC System	On-board H2 Storage	Hybrid Battery
<ul> <li>80 kW<sub>net</sub> Stack Membrane Electrode GDL/MPL Bipolar Plate Seal &amp; Gasket Balance of Stack</li> <li>BOP</li> </ul>	<ul> <li>Type IV Composite Tank</li> <li>Fill Port</li> <li>High Pressure Regulator</li> <li>Valves &amp; Sensors</li> <li>Fittings &amp; Piping</li> <li>Assembly &amp; Inspection</li> </ul>	• Li-Ion hybrid battery (40kW, 1.2kWh)
<ul> <li>Fuer Management Thermal Management Air Management</li> <li>Water Management</li> <li>Balance of System Control Board Valves &amp; Sensors Fittings &amp; Piping Wire Harness Others</li> </ul>	Compressed Hydrogen Storage	PEM Fuel Cell System Li-lon Battery Pack
<ul> <li>Assembly, QC, and Conditioning</li> </ul>	Fuel Cell Hybrid Electri	ic Vehicle Power System



### **PEMFC System** 80 kW<sub>net</sub> PEM Fuel Cell System *Preliminary System Design*

# The 80 kW<sub>net</sub> direct hydrogen PEM fuel cell system configuration was referenced in previous and current studies conducted by Argon National Laboratory (ANL).



80 kW<sub>net</sub> Fuel Cell System Schematic<sup>1</sup>

1. DOE Fuel Cell Technologies Program Record, "Fuel Cell System Cost -2012" 2. R. K. Ahluwalia, X. Wang, and R. Kumar, "Fuel cells systems analysis," 2012 DOE Hydrogen Program Review, Washington DC, May 14-18, 2012.

#### Key Parameters Stack • 3M NSTFC MEA • 25 μm supported membrane • 0.196 mg/cm<sup>2</sup> Pt

- Power density: 984 mW/cm<sup>2</sup>
- Metal bipolar plates
- Non-woven carbon fiber GDL

#### Air Management

- Honeywell type compressor /expender
- Air-cooled motor / Air-foil bearing

#### Water Management

- Cathode planar membrane humidifier with pre-cooler
- No anode humidifier

#### **Thermal Management**

Micro-channel HX

#### **Fuel Management**

• Parallel ejector / pump hybrid



Based on ANL's stack performance analysis, we made the following system and material assumptions for the cost estimation.

Stack Components	Unit	Current System	Comments
Production volume	systems/year	500,000	High volume
Stacks' net power	kW	80	DOE 2012
Stacks' gross power	kW	88	DOE 2012
Cell power density	mW/cm <sup>2</sup>	984	DOE 2012
Peak stack temp.	Degree C	87	DOE 2012
Peak stack pressure	Bar	2.5	DOE 2012
System Voltage (rated power)	Volt	300	DOE 2012
Platinum price	\$/tr.oz.	\$1,100	DOE 2012
Pt loading	mg/cm <sup>2</sup>	0.196	DOE 2012
Membrane type		Reinforced 3M PFSA	
Membrane thickness	micro meter	25	
GDL layer		None-woven carbon paper	
GDL thickness	micro meter	185	@50 kPa pressure
MPL layer thickness	micro meter	40	
Bipolar plate type		76Fe-20Cr-4V with nitridation surface treatment	
Bipolar plate base material Thickness	micro meter	100	
Seal material		Viton®	

# Pt price was \$1,100/tr.oz. for the baseline, which was consistent with other DOE cost studies.



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# We assumed a double-side dispersion coating process (US 2008/0269409) to an ePTFE-supported membrane process.

	ePTFE	3M PFSA Supported Membrane
Thickness (µm)	25	25
Porosity (%)	95%	-
Bulk Density (g/cm <sup>3</sup> )	0.098	1.97
Material Cost	\$5/m <sup>2</sup>	3M Ionomor:\$80/lbs*



The reinforced 25  $\mu m$  3M PFSA membrane is estimated to cost ~\$19/m² on an active area basis, with materials representing ~85% of the cost.

Membrane Manufactured Cost <sup>1</sup>					
Component	Material		Process		
	(\$/m²)	(\$/kg)	(\$/m²)	(\$/kg)	
Film Handling	\$6.33	\$107.64	\$0.34	\$5.78	
Coating	\$10.07	\$171.11	\$0.44	\$7.42	
Drying & Cooling	\$0.00	\$0.00	\$1.98	\$33.64	
Quality Control	\$0.00	\$0.00	\$0.04	\$0.60	
Laminating	\$0.00	\$0.00	\$0.05	\$0.93	
Packaging	\$0.03	\$0.43	\$0.03	\$0.46	
Subtotal	\$16.42	\$279.19	\$2.87	\$48.83	
Total	19.30 (\$/m²)				
	328.02 (\$/kg)				



<sup>2</sup> 3M PFSA ionomer cost assumed to be \$80/lb based on FCTT feedback.

 $^3$  ePTFE cost assumed to be  $\fi)m^2$ 



Organic whisker support was fabricated by physical vapor deposition (PVD) with vacuum annealing process. Catalysts were coated to this layer via vacuum sputtering process.



The 2012 electrode cost estimate of \$86/m<sup>2</sup> which was dominated by Platinum price. We have assumed Pt price to be \$1,100/tr.oz. or \$35.4/g.

Manufactured Cost	Anode <sup>1</sup> (\$/m <sup>2</sup> )	Cathode <sup>1</sup> (\$/m <sup>2</sup> )	Total <sup>1</sup> (\$/m <sup>2</sup> )
Material	\$25.97	\$50.33	\$76.30
Capital Cost	\$1.79	\$2.94	\$4.73
Labor	\$0.16	\$0.19	\$0.35
Tooling	\$1.18	\$1.75	\$2.93
Other <sup>2</sup>	\$0.53	\$0.76	\$1.29
Total	\$29.63	\$55.97	\$85.60

 $^{1}$  m<sup>2</sup> of active area

<sup>2</sup> Other costs include utilities, maintenance, and building





We cost a non-woven carbon paper GDL with MPL based on discussions with formerly Ballard Material Products on their AvCarb® GDS3250 for automotive applications.





The non-woven carbon paper GDL (for *both* anode and cathode) cost about \$12/m<sup>2</sup>, on an active area basis.

Manufactured Cost <sup>1</sup>	GDL (\$/m²)	GDL (Anode + Cathode) (\$/m <sup>2</sup> )
Material	\$0.88	\$1.76
Capital Cost	\$1.86	\$3.71
Labor	\$0.31	\$0.63
Tooling	\$1.88	\$3.76
Other <sup>2</sup>	\$0.94	\$1.88
Total	\$5.87	\$11.73



<sup>1</sup> Manufactured cost on an active area basis

<sup>2</sup> Other costs include utilities, maintenance, and building

80 kW<sub>net</sub> PEMFC System Stack MEA Assembly Process

The anode and cathode organic whisker layers were hot pressed to the membrane with Teflon<sup>®</sup> backing sheets. GDL layers were laminated to the coated membrane and were formed an MEA in roll good form. The MEA was cut into sheets and molded with a frame seal.



#### The MEA with frame seal together were estimated to cost about \$128/m<sup>2</sup>.

Manufactured Cost <sup>1</sup>	MEA (\$/m²)	Frame Seal (\$/m <sup>2</sup> )	
Material - Membrane - Electrode - GDL	94.48 - 16.42 - 76.30 - 1.76	\$6.07	
Capital Cost	\$9.80	\$1.71	
Labor	\$1.15	\$1.24	
Tooling & Equipment	\$7.60	\$1.46	
Other <sup>2</sup>	\$3.63	\$0.70	
Subtotal	\$116.65	\$11.17	
Total	127.83		

<sup>1</sup> Manufactured cost on a per m<sup>2</sup> of active area basis

<sup>2</sup> Other costs include utilities, maintenance, and building

 $^{\rm 3}$  Active area to Total area ratio reduced from 85% to 75%, based on feedback from OEMs and FCTT





The metal bipolar plate cost was based on discussions with ORNL on their thermal nitriding process<sup>1</sup> for specific alloys, e.g. Fe-20Cr-4V.



- 1. Nitrided metallic bipolar plates, M.P. Brady, et al., ORNL, DOE Merit Review presentation, May 2009
- 2. US 20090081520 (Hitachi)
- 3. Discussion with Minster Press Inc., April 2010
- 4. Preferential thermal nitridation to form pin-hole free Cr-nitrides to protect proton exchange membrane fuel cell metallic bipolar plates, M.P. Brady, et al., Scripta Materialia 50 (2004) 1017-1022



The cost of the nitrided Fe-20Cr-4V metal bipolar plates was estimated to be ~\$57/m<sup>2</sup> or ~\$6/kW.

	Bipola Manufa Cost <sup>1</sup>	r Plate actured (\$/m <sup>2</sup> )	Bipola Manuf Cost <sup>2</sup>	ar Plate actured (\$/kW)	Bipolar Plate Manufactured Cost (\$57/m <sup>2</sup> )
Component	Material	Process	Material	Process	Others 10.5%
Stamping	\$25.02	\$11.06	\$2.78	\$1.23	
Laser Welding	\$0.00	\$8.73	\$0.00	\$0.97	Equipment & Tooling 16.3%
Nitridation	\$0.00	\$12.47	0.00	\$1.39	
Subtotal	\$25.02	\$32.26	\$2.78	\$3.58	
Total	\$57	7.28	\$6	5.36	Labor Cost 11.7%

**Capital Costs** 17.8%

<sup>1</sup> Manufactured cost on an active area basis

<sup>2</sup> Manufactured cost on a kW<sub>net</sub> basis

As a based material, Fe-20Cr-4V is a specialty metal and could have higher price than the conventional base materials, such as SS316, etc.



#### The cost of the gasket was estimated to be $\sim$ \$7/m<sup>2</sup>.

Manufactured Cost <sup>1</sup>	Gasket (\$/m²)
Material	\$0.62
Capital Cost	\$1.93
Labor	\$1.26
Tooling	\$1.86
Other <sup>2</sup>	\$1.18
Total	\$6.85

<sup>1</sup> Manufactured cost on an active area basis <sup>2</sup> Other costs include utilities, maintenance, and building



# Transfer molding was used to fabricate the seals between the MEA and bipolar/cooling plate. The seal material is Viton<sup>®</sup> which costs ~\$20/lb.



The 80 kW<sub>net</sub> PEM fuel cell stack cost \$24/kW. Electrodes, bipolar plates, and membranes were the top three cost drivers.

Stack Components	Stack Manufacturin g Cost (\$/kW)	Comments
Membrane	\$2.14	PFSA ionomer (\$80/lb)
Electrode	\$9.51	3M NSTFC
GDL	\$1.30	No-Woven carbon paper
Bipolar Plate	\$6.36	Nitrided metallic plates
Seal	\$2.00	Viton
BOS	\$0.55	Manifold, end plates, current collectors, insulators, tie bolts, etc.
Final Assembly	\$1.40	Robotic assembly
Stack Conditioning	0.60	2 Hours
Total stack <sup>2</sup>	23.85	



1. Stack assembly cost category included MEA assembly and stack QC; QC included visual inspection, and leak tests for fuel, air, and coolant loops.

2. Results may not appear to calculate due to rounding of the component cost results.



### The water management system OEM cost<sup>1,2</sup> was projected to be \$128.

Component	Factory Cost <sup>1</sup>	OEM Cost <sup>1,2</sup>
Cathode Planar Membrane Humidifier	112	128

- <sup>1</sup> R. K. Ahluwalia and X. Wang, Automotive Fuel Cell System with NSTFC Membrane Electrode Assemblies and Low Pt Loading, July 21, 2009
- <sup>2</sup> High-volume manufactured cost based on a 80 kW net power PEMFC system. Does not represent how costs would scale with power (kW).
- <sup>3</sup> Assumes 15% markup to the automotive OEM for BOP components



### The cathode planar membrane humidifier cost was estimated using bottom-up costing tools.



#### The thermal management system OEM cost<sup>1,2</sup> was projected to be \$404.

Component	Factory Cost <sup>1</sup>	OEM Cost <sup>1,2</sup>
HT Radiator	86	99
LT Radiator	21	25
Air Precooler	-	20
HT/LT Radiator Fan	-	75
- Motor	-	- 60
- Fan	-	- 15
HT Coolant Pump	-	150
- Motor	-	- 95
- Pump	-	- 55
LT/Air Precooler Coolant Pump	-	30
Other	-	5
Total	387	404





<sup>1</sup> High-volume manufactured cost based on a 80 kW net power PEMFC system. Does not represent how costs would scale with power (kW). <sup>2</sup> Assumes 15% markup to the automotive OEM for BOP components

# The air precooler, radiator fan, coolant pumps, and their motors were assumed to be purchased components; hence their price included a markup.



#### The fuel management system OEM cost<sup>1,2</sup> was projected to be \$382.

Component	Factory Cost <sup>1</sup>	OEM Cost <sup>1,2</sup>
H <sub>2</sub> Blower	219.5	252
H <sub>2</sub> Ejectors	-	20
H <sub>2</sub> Demister	-	61
Solenoid Valves	-	23
Purge Valve	13	15
Check valve	9	10
Total	346	382



Parker Hannifin Brochure for Model 55 Univane<sup>™</sup> Compressor

<sup>1</sup> High-volume manufactured cost based on a 80 kW net power PEMFC system. Does not represent how costs would scale with power (kW).

<sup>2</sup> Assumes 15% markup to the automotive OEM for BOP components

#### The H<sub>2</sub> ejectors, H<sub>2</sub> demister, and solenoid valves were assumed to be purchased components; hence their price included a markup.



### The air management system OEM cost<sup>1,2</sup> was projected to be \$936.

Component	Factory Cost <sup>1</sup>	OEM Cost <sup>1,2</sup>
CEM (Compressor, Expander, Motor, Motor Controller	535	615
Air demister	-	156
Air/H <sub>2</sub> mixer	-	27
Flow orifice	-	5
Air filter	-	4
Total	-	936



CEM: Honeywell, DOE Program Review, Progress Report & Annual Report, 2005

<sup>1</sup> High-volume manufactured cost based on a 80 kW net power PEMFC system. Does not represent how costs would scale with power (kW). <sup>2</sup> Assumes 15% markup to the automotive OEM for BOP components

# The air demister, $air/H_2$ mixer, flow orifice, and air filter were assumed to be purchased components; hence their price included a markup.



The 80 kW<sub>net</sub> PEM fuel cell system cost \$53/kW at the mass production volume. Stack, air management, and thermal management were the top three cost drivers.

System Components	System Manufacturing Cost (\$/kW)	Comments	80 kW <sub>net</sub> PEM Fuel Cell System Cost (\$4,256/system) System Assembly 7.4%
Stack	\$23.87		Balance of System 7.3%
Water management	\$1.6	Cathode side humidifier, etc.	Fuel Management 9.0%
Thermal management	\$5.0	HX, coolant pump, etc.	44.8
Air management	\$10.1	CEM, etc.	Air Management
Fuel management	\$4.8	H2 pump, etc.	19.0% Water
Balance of system	\$3.9	Sensors, controls, wire harness, piping, etc.	Thermal Management Management 3.0% 9.5%
System assembly	\$3.9		
Total system <sup>1, 2</sup>	\$53.2		

- 1. Assumed 15% markup to the automotive OEM for BOP components
- 2. Results may not appear to calculate due to rounding of the component cost results.

#### The 80 kW<sub>net</sub> direct hydrogen PEM fuel cell system cost \$4,256 at the mass production volume.



Stack 44.8% The 5,000 PSI type IV compressed hydrogen tank design was referenced in studies TIAX conducted on hydrogen storage<sup>1, 2</sup>.



Compressed Hydrogen Storage System Schematic<sup>1, 2</sup>

- 1. E. Carlson and Y. Yang, "Compressed hydrogen and PEM fuel cell system," Fuel cell tech team freedomCar, Detroit, MI, October 20, 2004.
- S. Lasher and Y. Yang, "Cost analysis of hydrogen storage systems Compressed Hydrogen On-Board Assessment – Previous Results and Updates for FreedomCAR Tech Team", January , 2007

#### **Key Parameters** System Pressure: 5.000 PSI Single Tank Design • Usable H2: 5.6 kg Safety Factor: 2.25 Tank Carbon Fiber: Toray T700S Carbon Fiber Cost: \$12/lbs Carbon Fiber / Resin Ratio: 0.68: 0.32 (weight) Translational Strength Factor: 81.5% Fiber Process: Filament Winding Liner: HDPE **Pressure Regulator** In-tank

### The single tank design had a usable hydrogen storage capacity of 5.6 kg.



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### Assumptions for the hydrogen storage tank design were based on the literature review and third-party discussions.

Stack Components	Unit	Current System	Comments
Production volume	systems/year	500,000	High Volume
Usable hydrogen	Kg	5.6	
Recoverable H2 in the tank		IV	With HDPE liner
Tank type		IV	With HDPE liner
Tank pressure	PSI	5,000	
# of tanks	Per System	1	
Safety factor		2.25	
Tank length/diameter ratio		3:1	
Carbon fiber type		Toray T700S	
Carbon fiber cost	\$/lbs	12	
Carbon fiber vs. resin ratio		0.68:0.32	Weight
Carbon fiber translational		01 50/	
Strength factor		01.5%	
Damage resistant outer layer		S Class	Could be replaced
material		3-01a55	by cheaper E-glass
S-Glass cost	\$/lbs	7	
Impact resistant end dome		Digid Ecom	
material		nigiu ruaiti	
Rigid foam cost	\$/kg	3	
Liner material		HDPE	
Liner thickness	Inch	1/4	
In tank regulator cost	\$/unit	150	



### A vertically integrated manufacturing process was assumed for the tank and BOP components.

Major Tank Components	Major BOP Components	
Aluminum End Boss	In-tank primary pressure regulator	
HDPE liner	Valves & sensors	
Carbon fiber composite layer	Filling interface	
Glass fiber composite layer	Pressure release devices	
End domes (rigid foam)	Piping & fitting	



In the 5,000 PSI baseline system, the carbon fiber composite layer was the dominant cost driver.

System Components	2012 System Manufacturing Cost (\$/kWh)	Comments
Hydrogen	0.09	5.9 kg H2
Pressure Tank	12.69	
- Liner	- 0.09	
- Carbon fiber layer	- 11.79	Pre-preg carbon fiber cost \$36/kg
- Glass fiber layer	- 0.59	φ00/Ng
- Foam	- 0.22	
Primary pressure regulator	0.80	In-tank design
Valves & sensors	0.86	4 valves, 1 temperature sensor, 1 pressure sensor
Fill port	0.43	
Fittings, piping, safety device, etc.	0.64	Pressure relive valve, burst valve, etc.
Assembly & inspection	0.88	Including pressure test
Total system <sup>2</sup>	16.39	



# The 5,000 PSI compressed hydrogen storage tank system cost \$3,058 at the mass production volume.



### A lithium-ion battery pack will provide hybridization of a fuel cell vehicle which will improves fuel economy as well as having the function as a startup battery.



A vertically integrated manufacturing process was assumed for the four-level battery pack fabrication: electrode, cell, module, and pack.





The lithium-ion battery system cost \$862 /kWh. Battery management system and packaging have higher cost contributions.

Cost Category	Cell Cost (\$/cell)	Pack Cost (\$/pack)
Material	\$7.88	\$775
Labor	\$1.51	\$116.96
Equipment & tooling	\$1.38	\$48.03
Utility	\$0.79	\$26.76
Maintenance	\$0.67	\$23.79
Capital cost	\$1.18	\$37.85
Building	\$0.15	\$5.72
Total	\$13.56	\$1,033.83
Total (\$/kWh)*	\$327.63	\$861.52



\* Based on usable energy (1.88 kWh x 0.8 x0.8 = 1.2 /kWh )

### The 1.2 kWh lithium-ion battery system cost \$1,034 per pack at the mass production volume.



### Conclusion

### The overall PEM fuel cell system, onboard hydrogen storage, and hybrid battery costs are approximately \$8,318 per vehicle.



- The mass production manufacturing cost of the 80 kW<sub>net</sub> PEMFC stack was estimated to be \$23.8/kW.
- The mass production OEM cost of the 80 kW<sub>net</sub> PEMFC system was estimated to be \$53.2/kW
- The 5.6kg compressed on-board hydrogen storage system was estimated to be \$16.4/kWh at the mass production.
- The hybrid lithium-ion battery (40kW, 1.2kWh) costs \$1,034 per pack.



### **Thank You!**

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