



Cost Analysis of Direct Hydrogen PEM Fuel Cell/Lithium Ion Battery Hybrid Power Source for Transportation

2011 Fuel Cell Seminar, Orlando

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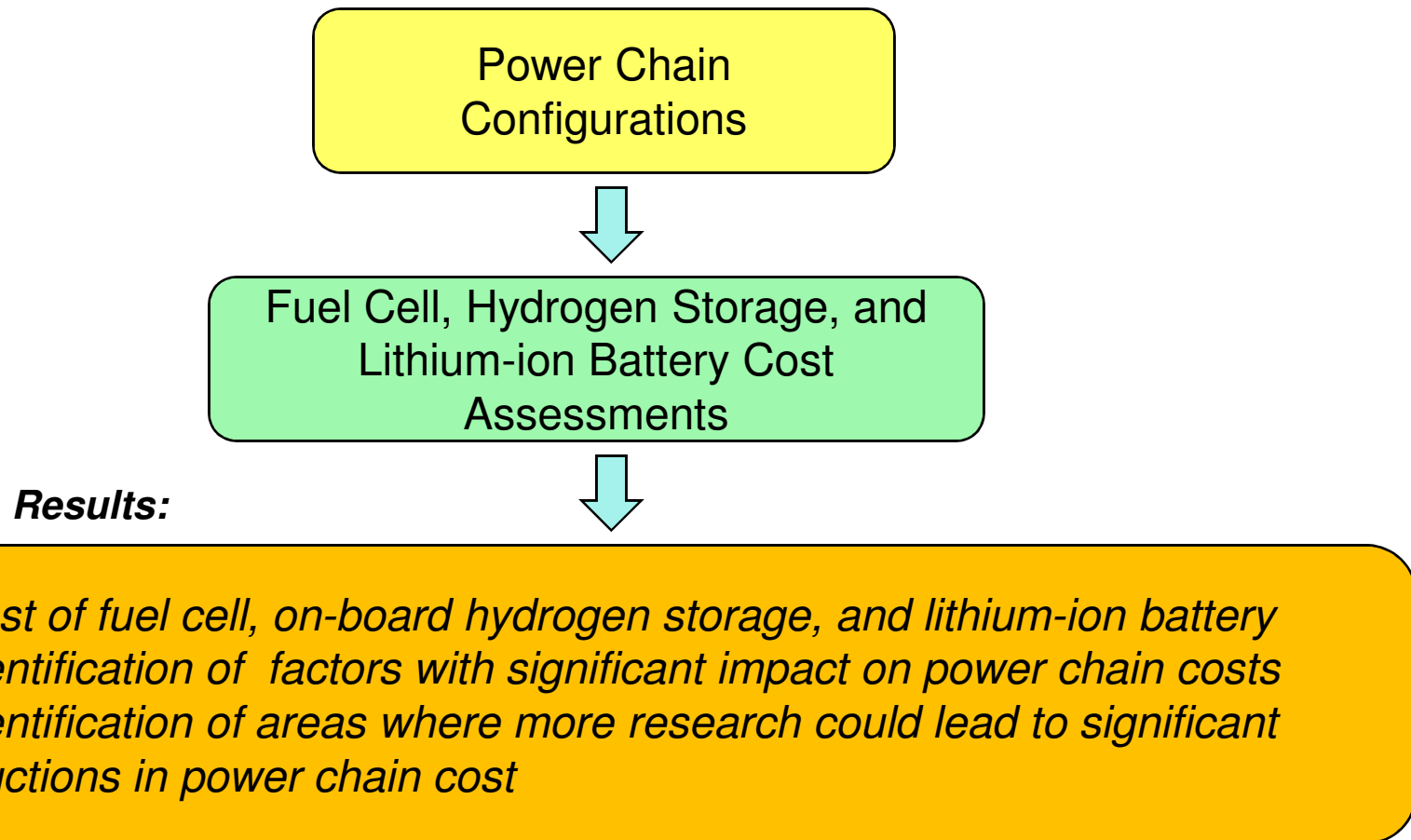
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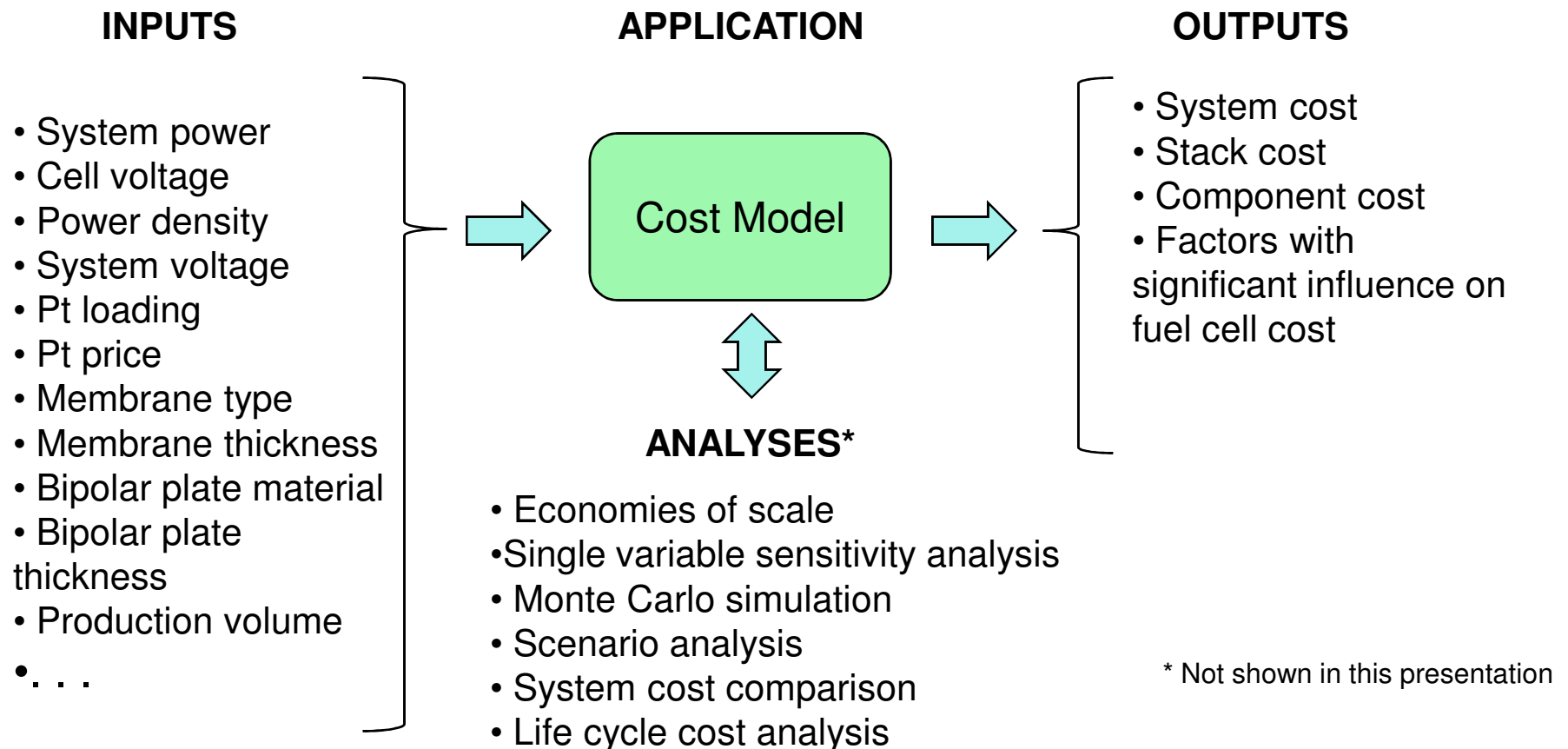
Objective

The due diligence objective was to assess the cost implications of a PEM fuel cell/lithium-ion battery hybrid power chain for mid-size passenger vehicles.



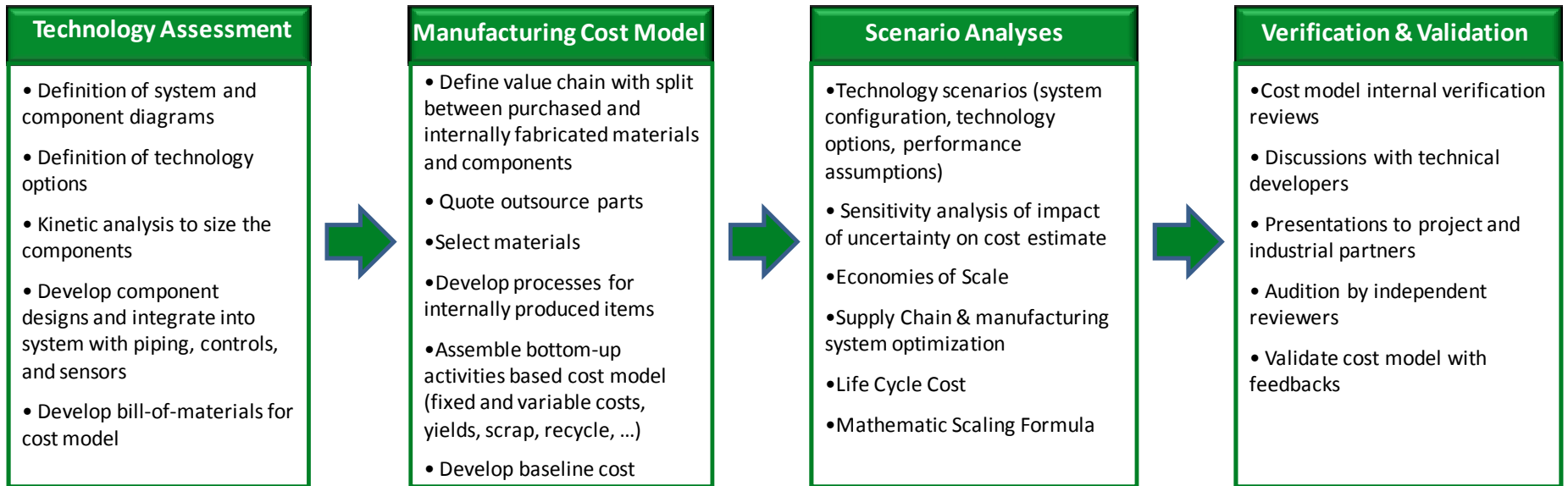
Approach

We employed a parametric approach in which Austin Power Engineering's manufacturing cost model was applied many times with different sets of input parameters.

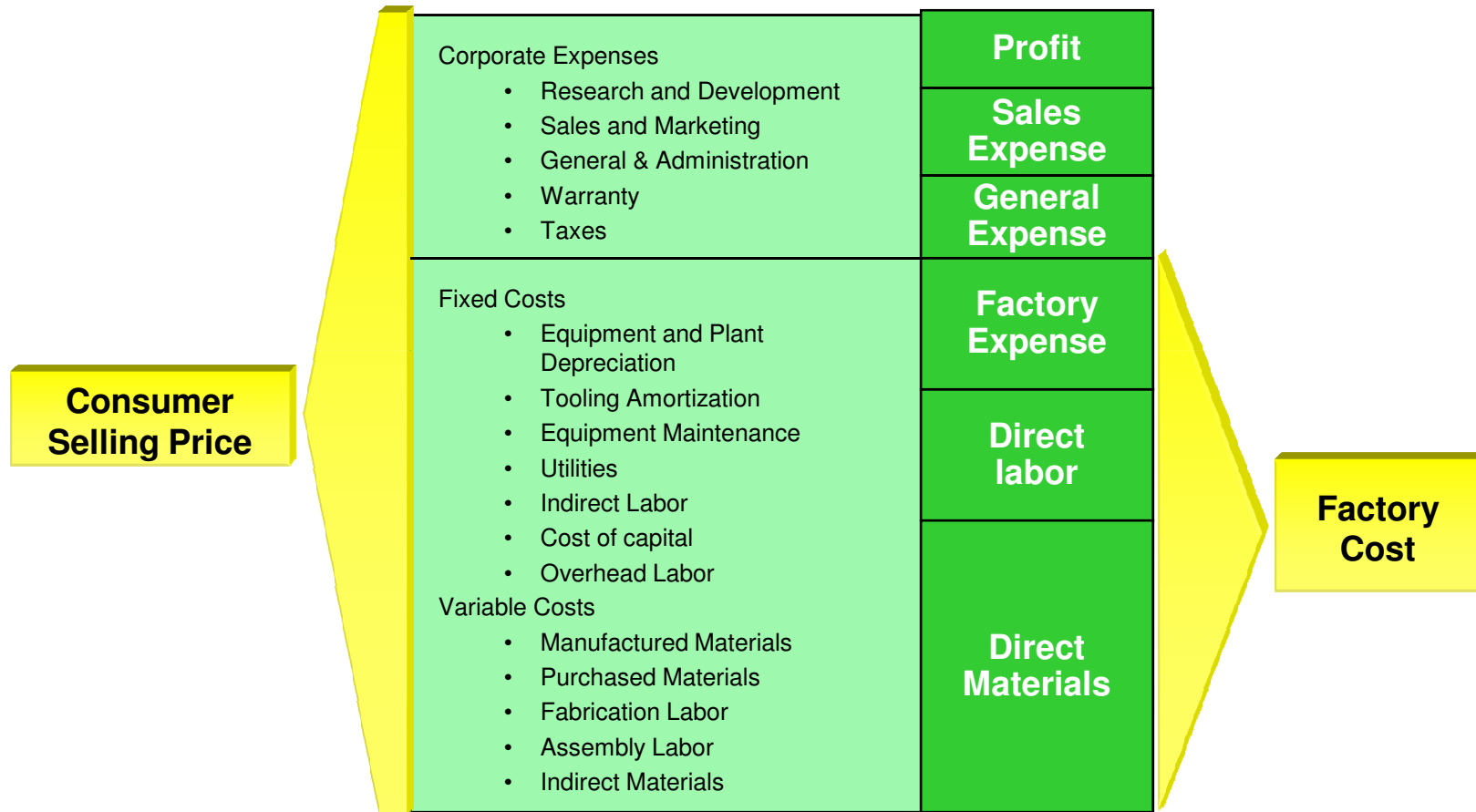


The information used in this presentation was publicly available, which was mainly from DOE reports, patents, journal papers, etc.

This approach has used successfully for estimating the cost of various technologies for commercial clients and the DOE.

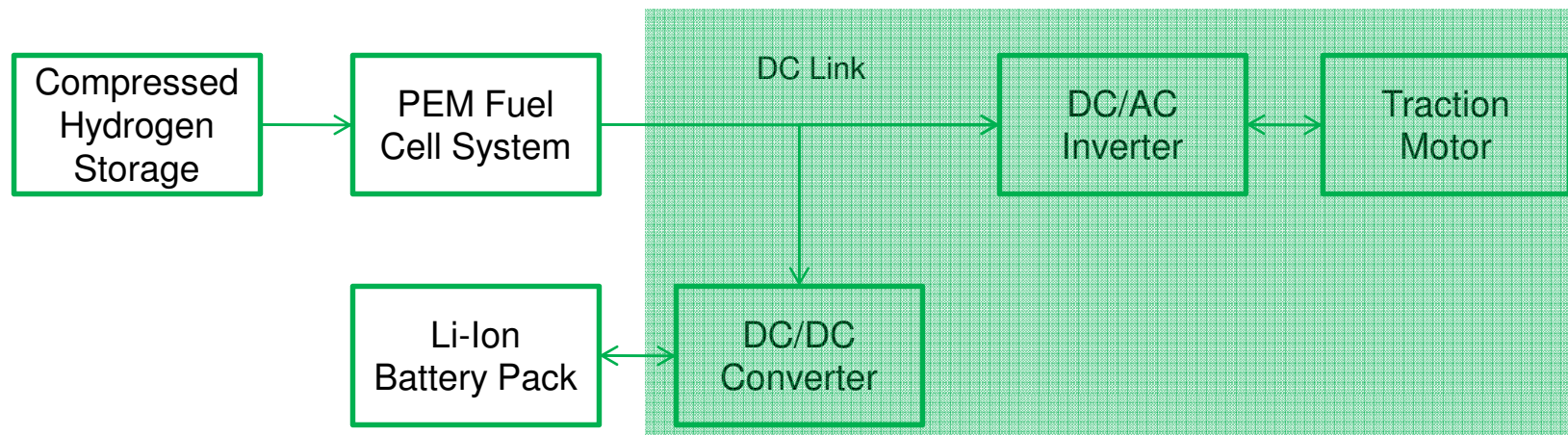


Austin Power Engineering's manufacturing cost models can be used to determine the fully loaded selling price to the consumer at high or low volumes.



We assume 100% financing with an annual discount rate of 10%, a 10-year equipment life, and a 25-year building life.

The bottom-up cost analysis included the PEM fuel cell system, compressed hydrogen storage tank, and lithium-ion battery pack.



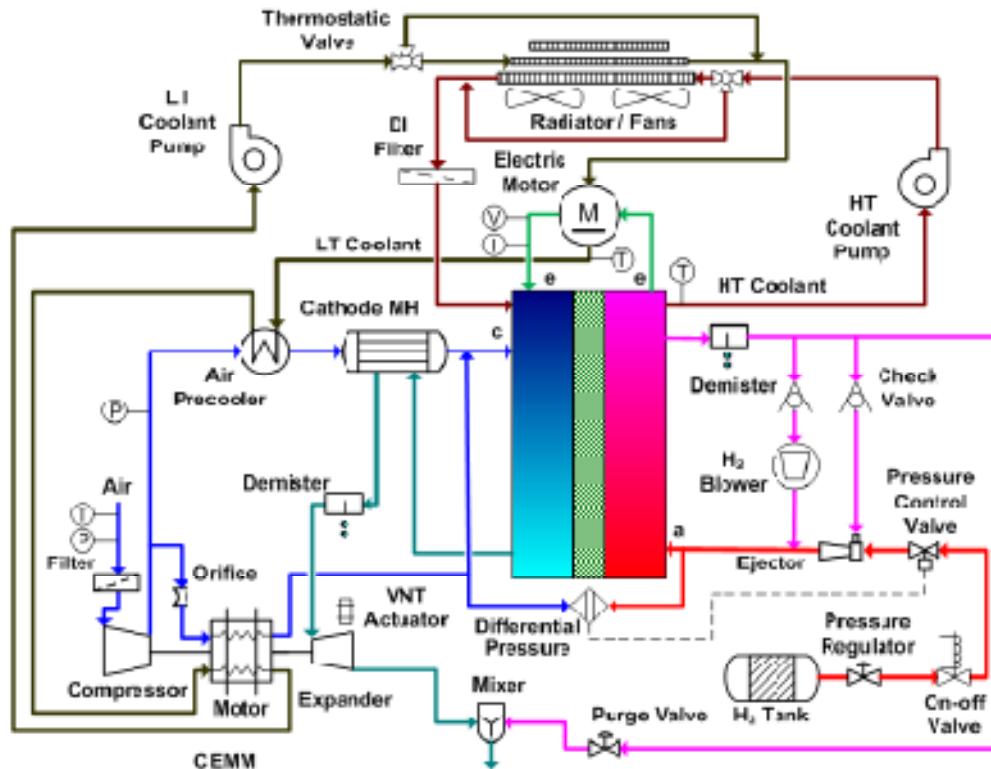
Fuel Cell Hybrid Vehicle Power Chain^{1~4}

To be included in the future study.

1. R. K. Ahluwalia, and X. Wang, "Direct hydrogen fuel cell systems for hybrid vehicles," *Journal of Power Sources* 139 (2005): 152-164.
2. P. Bubna, D. Brunner, S. G. Advani, and A. K. Prasad, "Prediction-based optimal power management in a fuel cell/battery plug-in hybrid vehicle," *Journal of Power Sources* 195 (2010): 6699-6708.
3. L. M. Fernandez, P. Garcia, C. A. Garcia, and F. Jurado, "Hybrid electric system based on fuel cell and battery and integrating a single dc/dc converter for a tramway," *Energy Conversion and Management* 52 (2011): 2183-2192.
4. J. Bernard, M. Hofer, U. Hannesen, A. Toth, A. Tsukada, F. Buchi, and P. Dietrich, "Fuel cell/battery passive hybrid power source for electric powertrains," *Journal of Power Sources*.

The bottom-up costs of the power electronic components (e.g., traction motor, inverter, and converter) will be included in a future study.

The 65 kW_{net} direct hydrogen PEM fuel cell system configuration was referenced in previous and current studies conducted by Argon National Laboratory (ANL).



65 kW_{net} Fuel Cell System Schematic¹

1. R. K. Ahluwalia, and X. Wang, "Direct hydrogen fuel cell systems for hybrid vehicles," *Journal of Power Sources* 139 (2005): 152-164.
2. R. K. Ahluwalia, X. Wang, and R. Kumar, "Fuel cells systems analysis," 2011 DOE Hydrogen Program Review, Washington DC, May 9-13, 2011.

Key Parameters

Stack

- 3M NSTFC MEA
- 20 μm supported membrane
- 0.05 (a)/0.1 (c) mg/cm² Pt
- 75 °C, 1.5 atm
- Metal bipolar plates
- Non-woven carbon fiber GDL

Air Management

- CEM module
- Air-cooled motor / Air-foil bearing

Water Management

- Cathode planar membrane humidifier with pre-cooler
- No anode humidifier

Thermal Management

- Micro-channel HX

Fuel Management

- Parallel ejector / pump hybrid

Based on ANL’s stack performance analysis, we made the following system and material assumptions for the cost estimation.

Stack Components	Unit	Current System	Comments
Production volume	systems/year	500,000	High volume
Stacks’ net power	kW	65	
Stacks’ gross power	kW	72	
Stacks’ gross power density	mW/cm ²	930	
Max. Stack Temp.	Degree C	90	
Platinum price	\$/tr.oz.	\$1,500	Last 5-year average
Pt Loading	mg/cm ²	0.15	
Membrane Type		Reinforced Nafion®	
Membrane Thickness	micro meter	20	
GDL Layer		None-woven Carbon Paper	
GDL Thickness	micro meter	185	@50 kPa pressure
MPL Layer Thickness	micro meter	40	
Bipolar Plate Type		76Fe-20Cr-4V with Nitridation Surface Treatment	
Bipolar Plate Base Material Thickness	micro meter	100	
Seal Material		Viton®	

Pt price was \$1,500/tr.oz. for the baseline. This was the average price for the last five years.

We used a bottom-up approach to determine the high-volume (500,000 units/year) manufacturing cost for the major stack and BOP components.

Major Stack Components

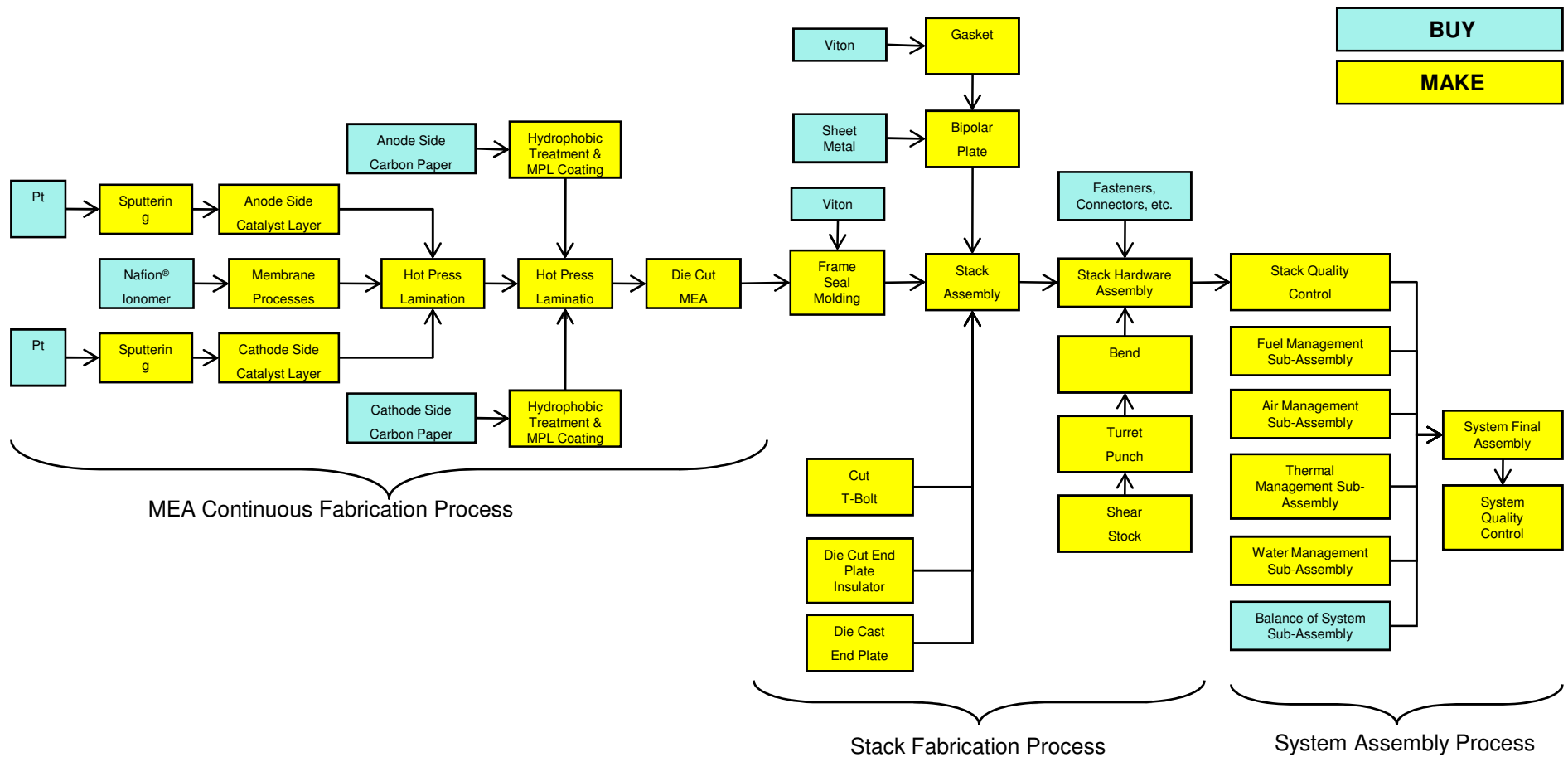
- Reinforced Membrane
- 3M NSTFC Type Electrodes
- Gas Diffusion Layer (GDL) with MPL Layers
- Membrane Electrode Assembly (MEA)
- Bipolar Plates
- Seals

Major BOP Components

- Micro-Channel Radiators (HT, LT)
- Cathode Planar Membrane Humidifier (MH)
- Compressor-Expander-Motor Module (CEM)
- H₂ Blower

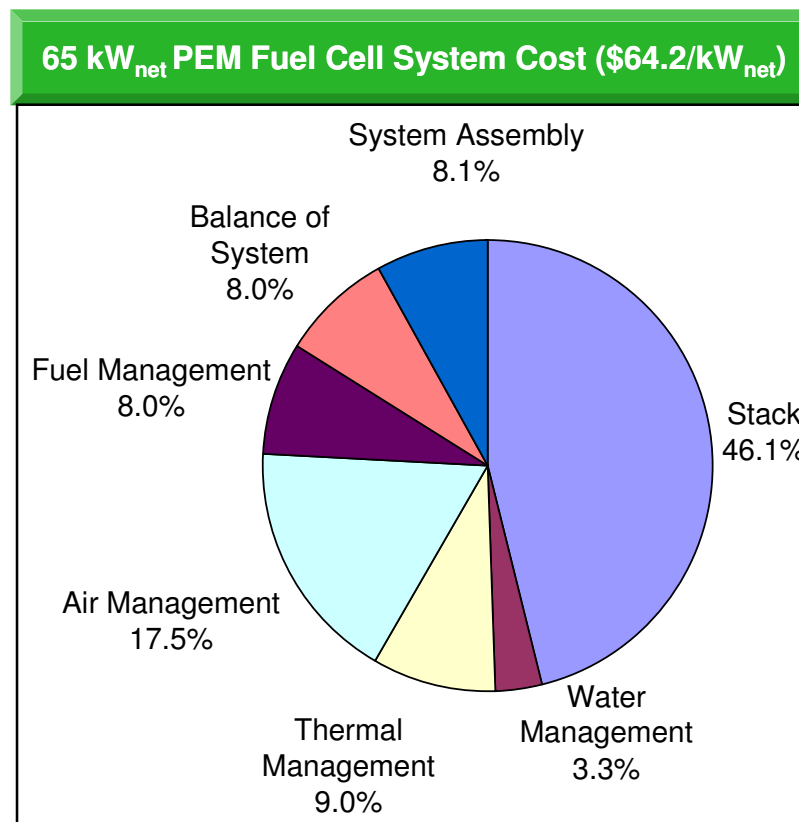
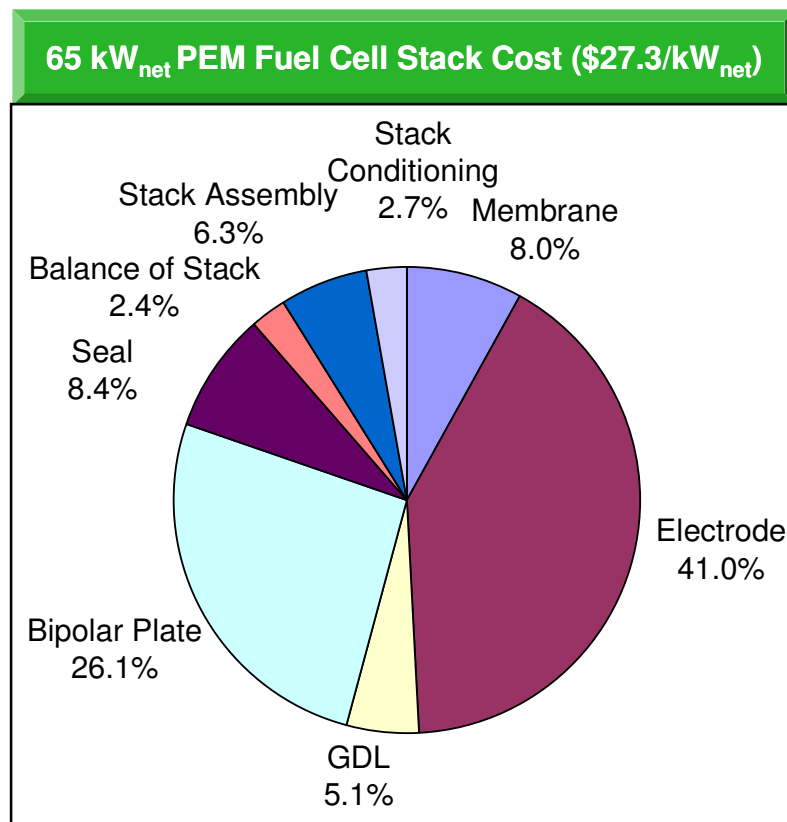
- Developed Bill of Materials (BOM)
- Developed production process steps for major components and sub-systems
- Used quotations / experience-based estimates for raw materials and off-shelve components
- Used the Austin Power Engineering technology cost model for major stack and BOP components
- Validated cost analysis from industrial feedbacks

A vertically integrated manufacturing process was assumed for the major stack and BOP components.



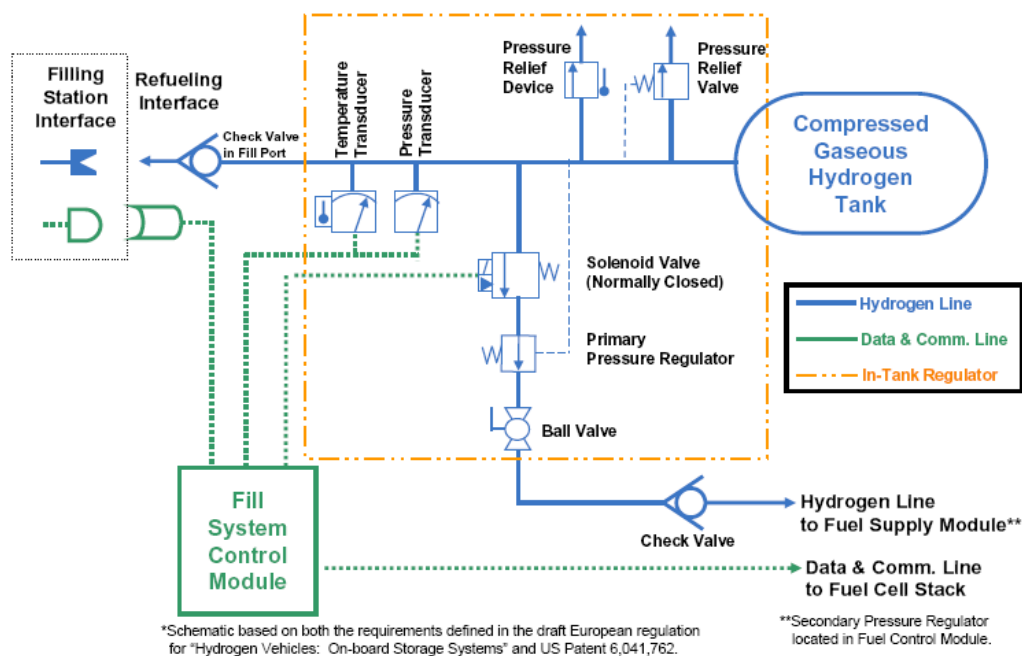
Supplier markups were included for the raw materials and purchased components.

The 65 kW_{net} PEM fuel cell stack cost \$27/kW. The electrode, bipolar plates, and seals were the top three cost drivers.



The 65 kW_{net} PEM fuel cell system cost \$64/kW. Stack, air management, and thermal management were the top three cost drivers.

The 5,000 PSI type IV compressed hydrogen tank design was referenced in studies TIAX conducted on hydrogen storage^{1, 2}.



Compressed Hydrogen Storage System Schematic^{1, 2}

Key Parameters

System

- Pressure: 5,000 PSI
- Single Tank Design
- Usable H₂: 5.6 kg
- Safety Factor: 2.25

Tank

- Carbon Fiber: Toray T700S
- Carbon Fiber Cost: \$12/lbs
- Carbon Fiber / Resin Ratio: 0.68 : 0.32 (weight)
- Translational Strength Factor: 81.5%
- Fiber Process: Filament Winding
- Liner: HDPE

Pressure Regulator

- In-tank

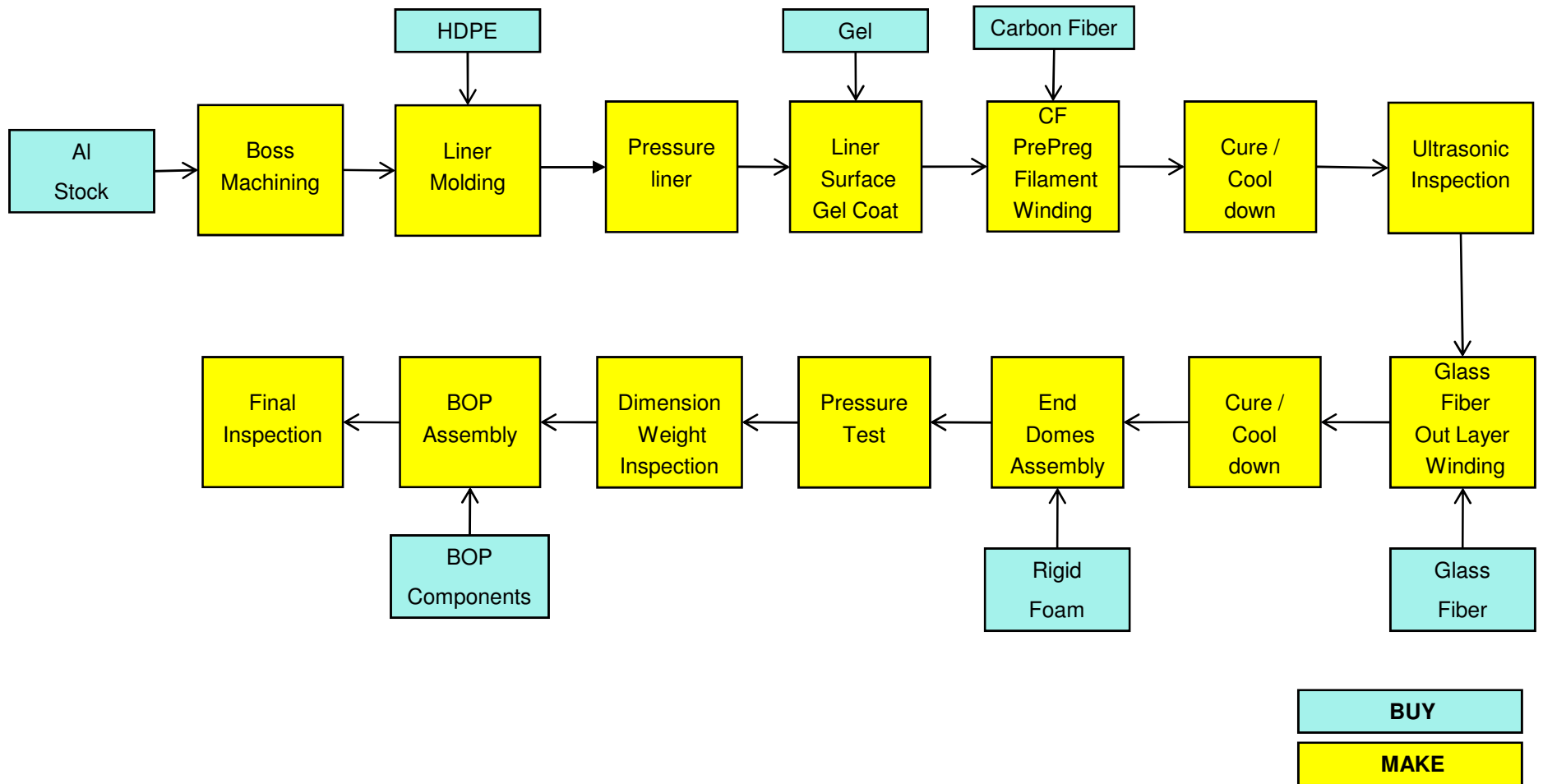
1. E. Carlson and Y. Yang, "Compressed hydrogen and PEM fuel cell system," Fuel cell tech team freedomCar, Detroit, MI, October 20, 2004.
2. S. Lasher and Y. Yang, "Cost analysis of hydrogen storage systems - Compressed Hydrogen On-Board Assessment – Previous Results and Updates for FreedomCAR Tech Team", January , 2007

The single tank design has a storage capacity of 5.6 kg usable hydrogen.

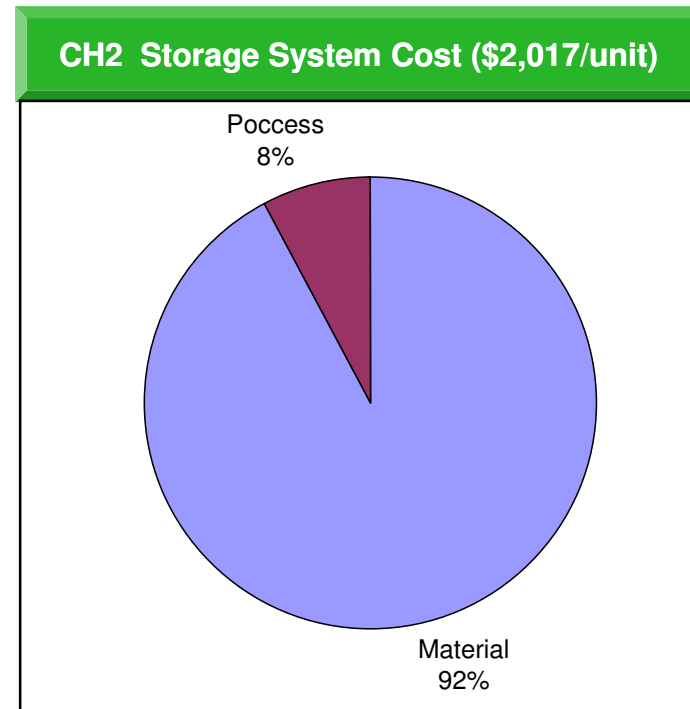
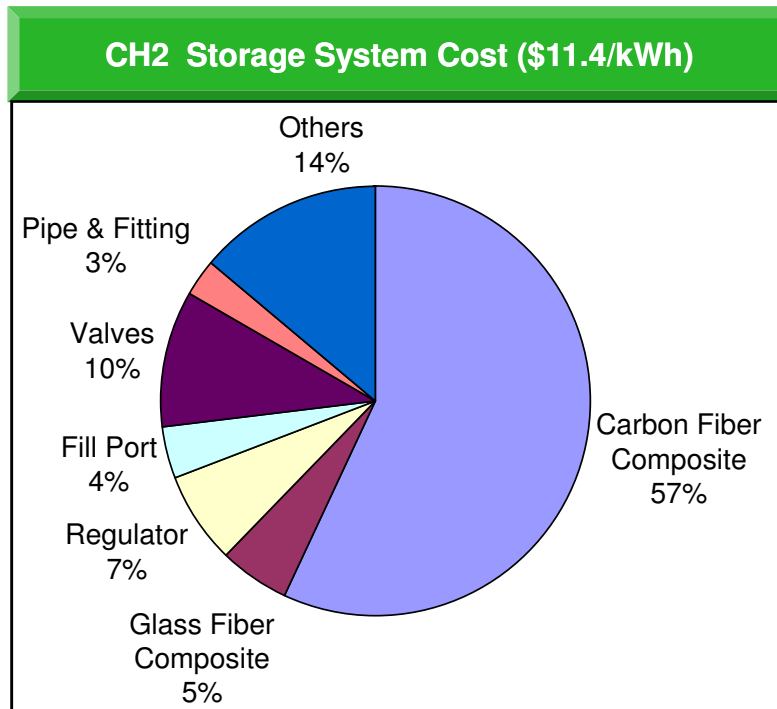
The assumptions for the hydrogen storage tank design were based on the literature review and third-party discussions.

Stack Components	Unit	Current System	Comments
Production volume	systems/year	500,000	High Volume
Usable Hydrogen	Kg	5.6	
Tank Type		IV	With HDPE liner
Tank Pressure	PSI	5,000	
# of Tanks	Per System	1	
Safety Factor		2.25	
Tank Length/Diameter Ratio		3:1	
Carbon Fiber Type		Toray T700S	
Carbon Fiber Cost	\$/lbs	12	
Carbon Fiber vs. Resin Ratio		0.68:0.32	Weight
Carbon Fiber Translational Strength Factor		81.5%	
Damage Resistant Outer Layer Material		S-Glass	Could be replaced by cheaper E-glass
S-Glass Cost	\$/lbs	7	
Impact Resistant End Dome Material		Rigid Foam	
Rigid Foam Cost	\$/kg	3	
Liner Material		HDPE	
Liner Thickness	Inch	1/4	
In Tank Regulator Cost	\$/unit	150	

A vertically integrated manufacturing process was assumed for the tank and BOP components.

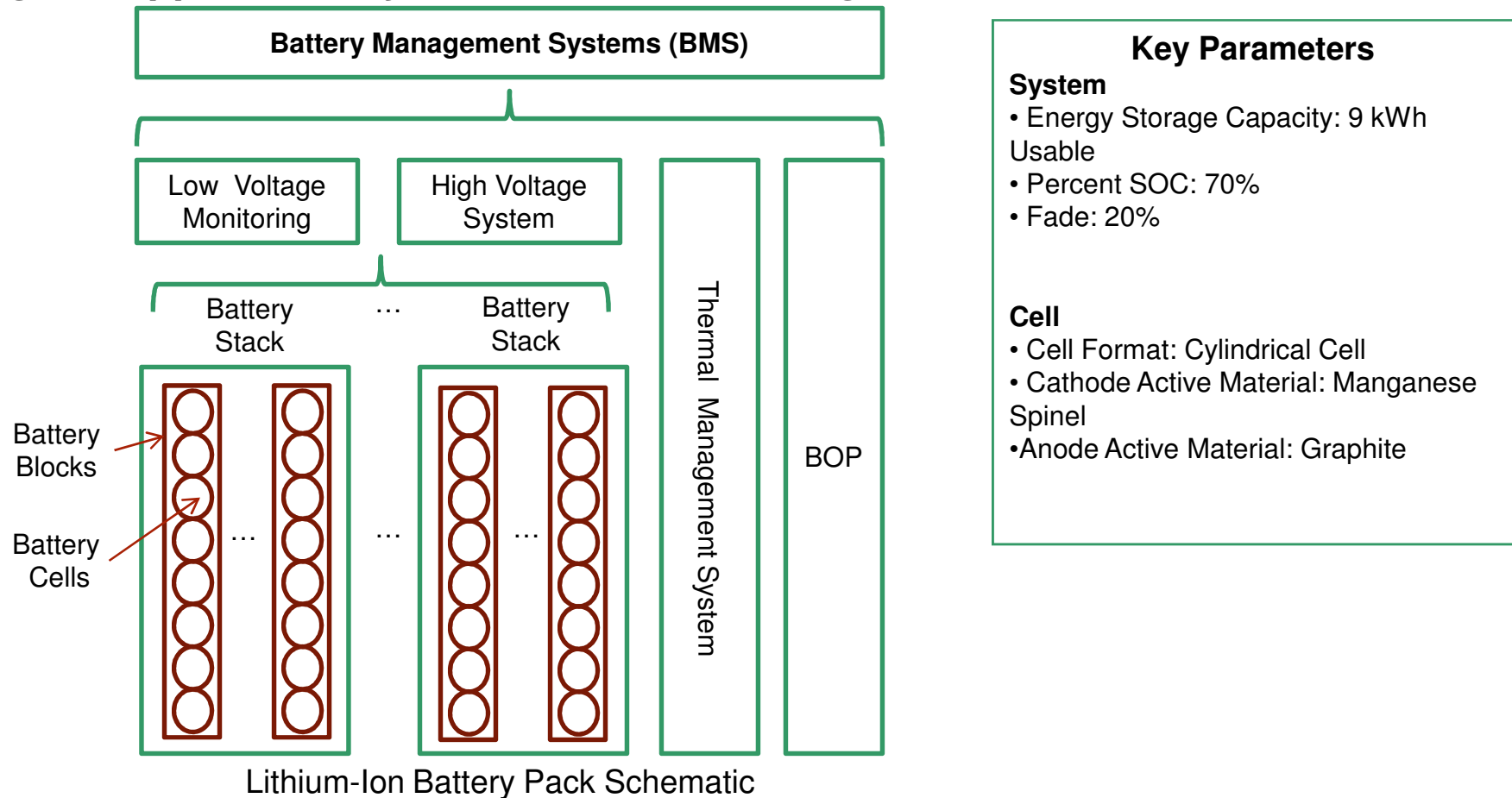


Material costs were a major cost driver. Cost reduction efforts need to focus on reducing material unit costs and weight.



In the 5,000 PSI baseline system, the carbon fiber layer is the dominant cost contributor.

A lithium-ion battery pack was designed to drive a mid-sized vehicles (~1,600 kg) for approximately 35 miles without using the fuel cell.

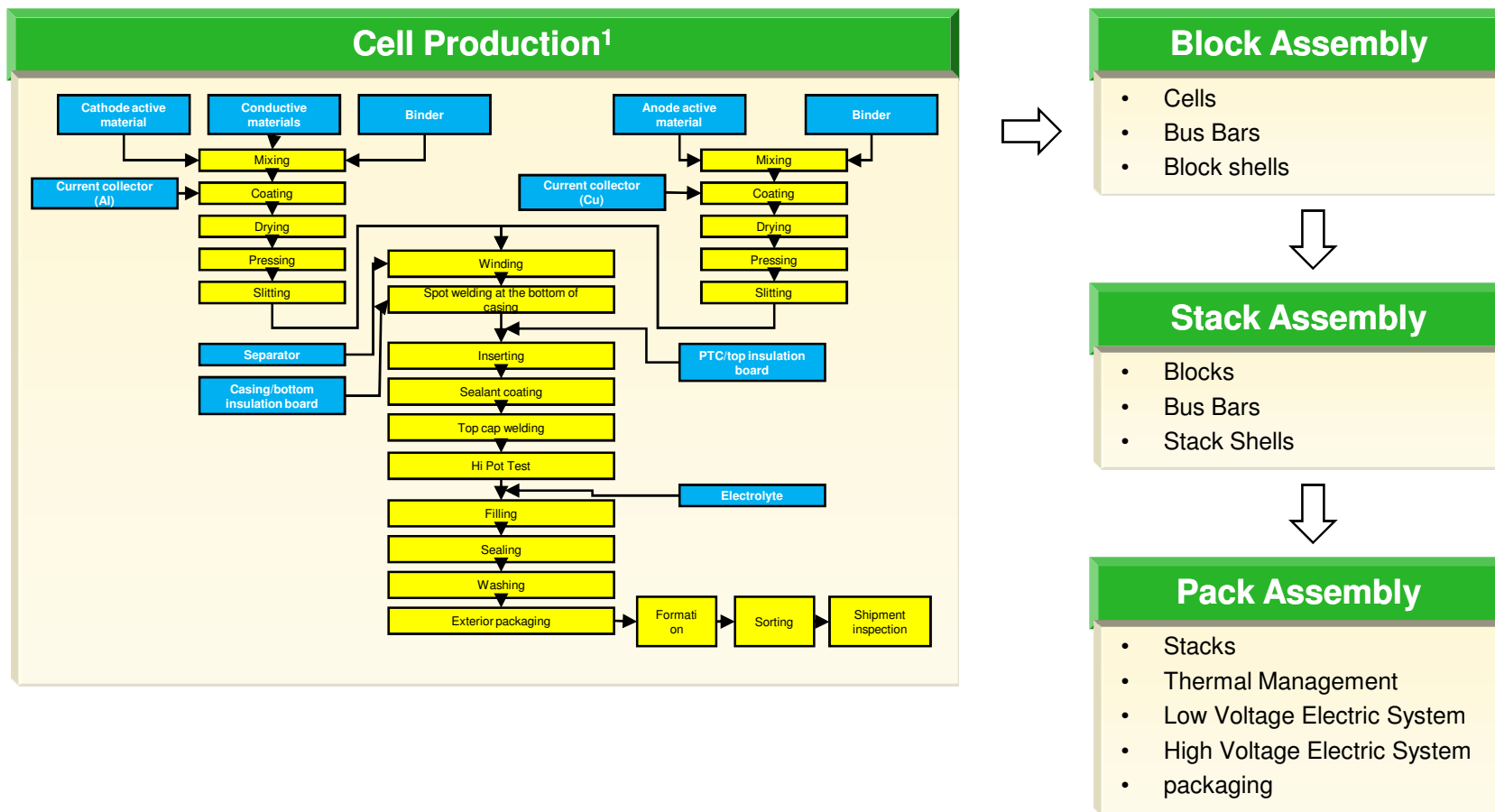


The battery blocks were repeat units containing battery cells and were used to assemble different size battery stacks.

The assumptions for the lithium-ion battery pack design were based on the literature review and third-party discussions.

Stack Components	Unit	Current System	Comments
Production volume	systems/year	500,000	
Gross Energy Storage Capacity	kWh	16	Applied SOC and Fade
Usable Energy Storage Capacity	kWh	9	
Percentage SOC	%	70	
Fade in Life	%	20	
Drive All Electric Range	Mile	~35	
Cell Type		Cylindrical Cell	
Anode Active Material		Graphite (MCMB 6-28)	
Cathode Active Material		LiMn ₂ O ₄	
Electrolyte Material		LiPF ₆	
Anode Current Collector Material		Cu	
Cathode Current Collector Material		Al	
Separator		Tri-layer PP/PE/PP	

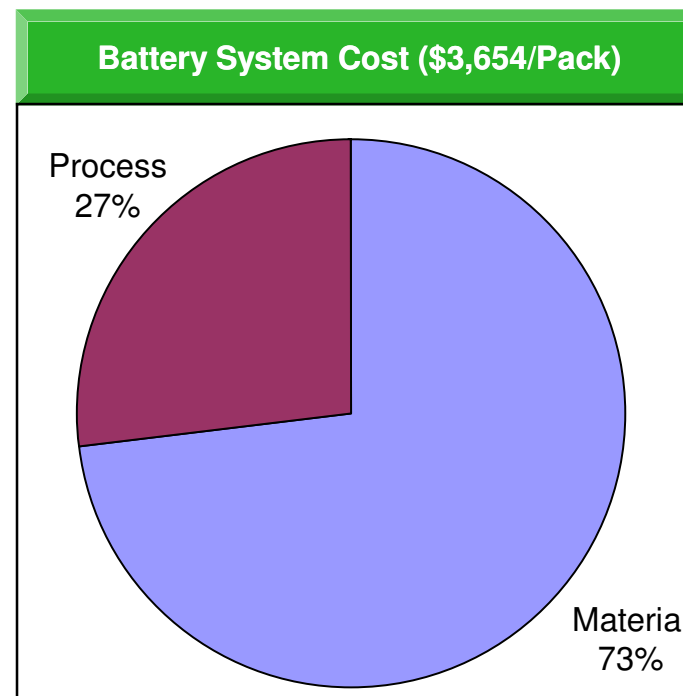
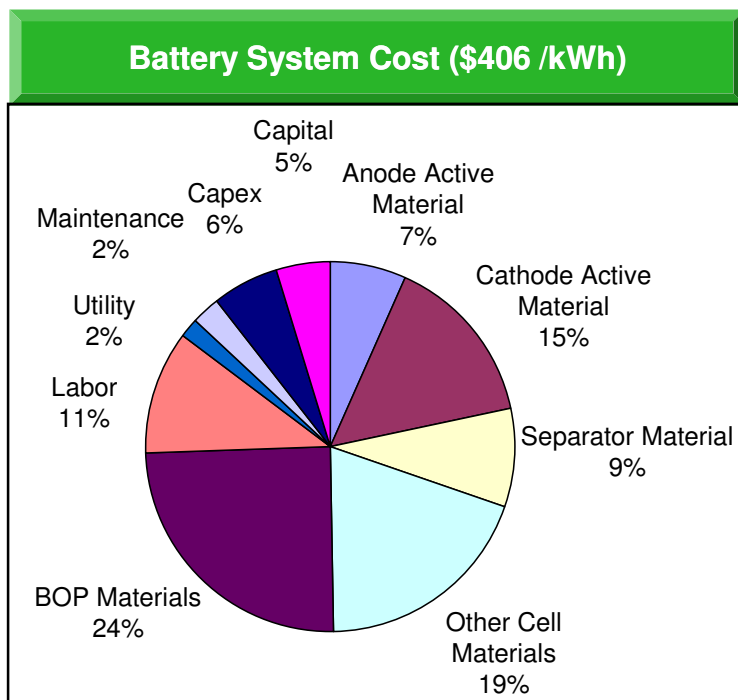
A vertically integrated manufacturing process was assumed for the four-level battery pack fabrication: cell, block, stack, and pack.



1. B., Barnett, Y. Yang, et al. "PHEV Battery Cost Assessment, PHEV Battery Costing Phase II", 2009 DOE Hydrogen Program Annual Merit Review, Arlington, VA

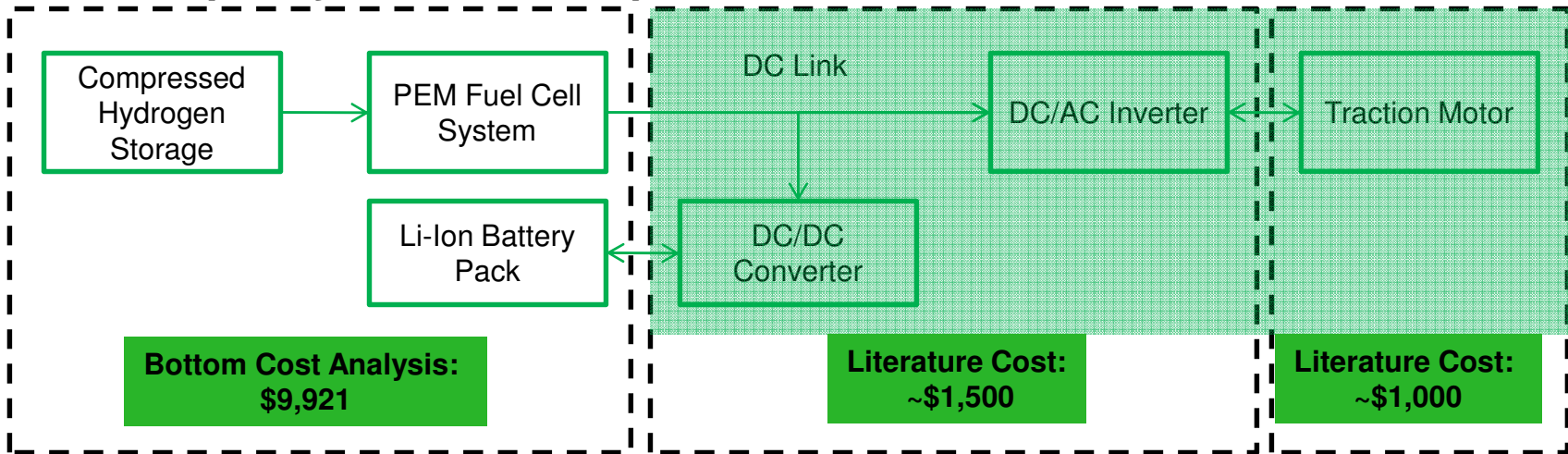
Lithium-Ion Battery Pack Preliminary Cost Results

The lithium-ion battery system cost \$406 /kWh. Of that, the material costs were approximately 70% and the process costs approximately 30%.

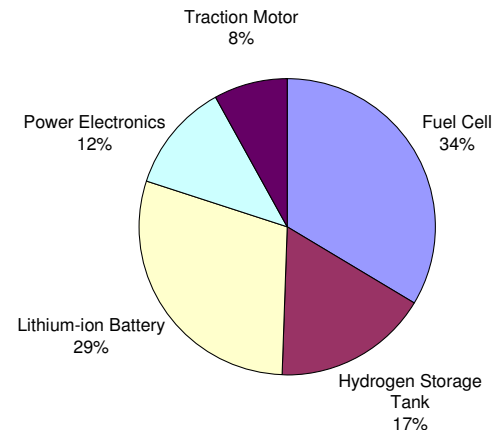


The lithium-ion battery system cost \$3,654 per pack.

The PEM fuel cell, on-board hydrogen storage, and lithium-ion battery pack cost \$9,921 per system at mass production volume.



Components	Unit Cost	System Cost
Fuel Cell	\$65 /kW	\$4,160
Hydrogen Storage Tank	\$11.4 /kWh	\$2,107
Lithium-ion Battery	\$406/kWh	\$3,654
Sub-total		\$9,921
Power Electronics	-	\$1,500
Traction Motor	-	\$1,000
Total		\$12,421



The complete PEM fuel cell/lithium-ion battery hybrid power chain cost \$12,421 per system.

Conclusions and Next Steps

The due diligence was preliminary. The following actions are needed to improve the current work:

- More analysis needs to be done, such as on power electronics, the traction motor, system modeling, sensitivity, and life cycles.
- Feedback from system integrators.
- Communication with component suppliers and equipment suppliers.
- Possible funding opportunities for the extended work.

Thank You!